

## **AMENDMENTS TO THE CLAIMS:**

The listing of claims will replace all prior versions, and listings of claims in the application:

### **LISTING OF THE CLAIMS**

1. (Original) In a method for treating an  $\text{NH}_3$ -containing gas wherein a gas containing an ammonia ( $\text{NH}_3$ ) of a high concentration is allowed to pass through a pre-treatment catalyst layer having a function for oxidizing  $\text{NH}_3$  to generate nitrogen monoxide (NO), and then pass through a denitration catalyst layer having a denitration function and a function for oxidizing  $\text{NH}_3$  to generate NO in combination; a method for preventing thermal deterioration of the catalyst, characterized by disposing a catalyst layer not having the function in the pre-treatment catalyst layer in parallel thereto.

**Please amend claims 2, 3, 4 and 5 as follows:**

2. (Currently Amended) The method according to claim 1, ~~wherein~~ wherein a part of a flow path section is composed of a catalyst layer containing an  $\text{NH}_3$  oxidation active component selected from zeolite, silica, titania, zirconia, alumina and the like supported with platinum (Pt), palladium (Pd), or rhodium (Rh); and another part of the flow path section is composed of a catalyst layer not containing the  $\text{NH}_3$  oxidation active component in the pre-treatment catalyst layer.

3. (Currently Amended) The method according to claim 1-~~or~~ 2, wherein the catalyst having the denitration function in combination with the function for oxidizing  $\text{NH}_3$  to generate NO contains titanium oxide ( $\text{TiO}_2$ ); an oxide of at least one of vanadium (V), tungsten (W) and molybdenum (Mo); and zeolite, titania, alumina, or zirconia supported with platinum (Pt).

4. (Currently Amended) The method according to ~~any one of claims 1 to 3~~ claim 1, wherein a feed amount of the  $\text{NH}_3$ -containing gas to the flow path of the catalyst layer having the function for oxidizing  $\text{NH}_3$  to generate NO in the pre-treatment catalyst and another flow path not having the former function is controlled in such that an  $\text{NH}_3$  concentration in the gas treated in the pre-treatment catalyst layer is higher than a NOx concentration.

5. (Currently Amended) The method according to ~~any one of claims 1 to 4~~ claim 1, wherein the gas containing the  $\text{NH}_3$  of the high concentration contains 3% of  $\text{NH}_3$ .

6. (Original) An apparatus for treating an  $\text{NH}_3$ -containing gas while preventing thermal deterioration of a catalyst, wherein a pre-treatment catalyst layer having a function for oxidizing  $\text{NH}_3$  to generate carbon monoxide (NO), and a catalyst layer having a denitration function in combination with another function for oxidizing  $\text{NH}_3$  to generate NO are sequentially disposed in a flow path section of a gas containing ammonia ( $\text{NH}_3$ ) along the gas flow direction, characterized in that a part of the flow path section is composed of a catalyst layer containing an  $\text{NH}_3$  oxidation active component selected from zeolite, silica, titania, zirconia and alumina supported with platinum (Pt), palladium (Pd), or rhodium (Rh); and another part of the flow path section is composed of a catalyst layer not containing the  $\text{NH}_3$  oxidation active component in the pre-treatment catalyst layer.

7. (Original) The apparatus according to claim 6, wherein a ratio of the catalyst layer containing the  $\text{NH}_3$  oxidation active component to the catalyst layer not containing the oxidation component is decided in the pre-treatment catalyst layer such that the  $\text{NH}_3$  concentration is higher than a NOx concentration in the outlet gas of the pre-treatment catalyst layer.

**Please insert the following new claims into the application:**

8. (New) The method according to claim 2, wherein the catalyst having the denitration function in combination with the function for oxidizing  $\text{NH}_3$  to generate NO contains titanium oxide ( $\text{TiO}_2$ ); an oxide of at least one of vanadium (V), tungsten (W) and molybdenum (Mo); and zeolite, titania, alumina, or zirconia supported with platinum (Pt).

9. (New) The method according to claim 2, wherein a feed amount of the  $\text{NH}_3$ -containing gas to the flow path of the catalyst layer having the function for oxidizing  $\text{NH}_3$  to generate NO in the pre-treatment catalyst and another flow path not having the former function is controlled in such that an  $\text{NH}_3$  concentration in the gas treated in the pre-treatment catalyst layer is higher than a  $\text{NO}_x$  concentration.

10. (New) The method according to claim 3, wherein a feed amount of the  $\text{NH}_3$ -containing gas to the flow path of the catalyst layer having the function for oxidizing  $\text{NH}_3$  to generate NO in the pre-treatment catalyst and another flow path not having the former function is controlled in such that an  $\text{NH}_3$  concentration in the gas treated in the pre-treatment catalyst layer is higher than a  $\text{NO}_x$  concentration.

11. (New) The method according to claim 2, wherein the gas containing the  $\text{NH}_3$  of the high concentration contains 3% of  $\text{NH}_3$ .

12. (New) The method according to claim 3, wherein the gas containing the  $\text{NH}_3$  of the high concentration contains 3% of  $\text{NH}_3$ .

13. (New) The method according to claim 4, wherein the gas containing the  $\text{NH}_3$  of the high concentration contains 3% of  $\text{NH}_3$ .